

COURSE OVERVIEW FE0570

API 579-1/ASME FFS-1: Fitness-for-Service (FFS) of Process Plant Equipment, Pressure Vessels, Piping & Storage Facilities

CEUS

(30 PDHs)

Course Title

API 579-1/ASME FFS-1: Fitness-for-Service (FFS) of Process Plant Equipment, Pressure Vessels, Piping & Storage Facilities

Course Date/Venue

July 28-August 01, 2024/TBA Meeting Room, The H Hotel, Sheikh Zayed Road, Dubai, UAE

Course Reference

FE0570

Course Duration/Credits Five days/3.0 CEUs/30 PDHs

Course Description









This course is designed to provide participants with a detailed and up-to-date overview of fitness-for-service (FFS) of process plant equipment, pressure vessels, piping and storage facilities in accordance with API 579-1/ASME FFS-1. It covers the API 579 and ASME FFS-1 standards; the fitness-for-service assessment procedure; the concept of remaining strength factor (RSF); the FFS and degradation mechanisms; the brittle fracture, pitting corrosion, blisters, HIC, SOHIC, distortion, crack-like flaws, creep, dent and gouges, laminations, wall thinning, cracking, embrittlement and mechanical damage; the FFS procedures and level of assessment; and the ASME FFS-1/API-579 procedure, API/ASME FFS levels of assessment, general FFS assessment procedure and failure prevention.

Further, the course will also discuss the piping codes B31, boiler and pressure vessel code sections, storage tanks, other codes and standards, post-construction codes and design margin piping systems; the FFS pipeline, piping, PV and tank; the systematic assessment of existing equipment for brittle fracture; and the brittle fracture features, brittle fracture and material behavior, brittle fracture risk factors and safeguards against brittle fracture.







During this interactive course, participants will learn the measurement of toughness visually; the critical exposure temperature, applicability and limitations of the procedure and data requirements; the assessment techniques and acceptance criteria; the remaining life assessment acceptability for continued service; the assessment of general metal loss and its applicability, limitations and inspection data/thickness measurements; the UT measurements, burst prevention, NDE data mapping and visual examination; the assessment of local thin area; the thickness readings, stress analysis and piping assessment; the proper assessment of pitting corrosion, laminations, weld misalignment, shell distortion, dents, gouges, crack-like flaws, creep and fire damage; the fitness for service assessment for a drilling platform structure and piping following fire damage; the assessment of hydrogen blisters and hydrogen damage as well as fatigue and API 574 piping inspection; and the risk-based inspection, inspection planning and equipment screening.

Course Objectives

Upon the successful completion of this course, each participant will be able to:-

- Apply and gain an in-depth knowledge on fitness-for-service (FFS) of process plant equipment, pressure vessels, piping and storage facilities in accordance with the latest API 579-1/ASME FFS-1 standard
- Discuss API 579-1 and ASME FFS-1 standards
- Carryout fitness-for-service assessment procedure and explain the concept of remaining strength factor (RSF)
- Determine FFS and degradation mechanisms, brittle fracture, pitting corrosion, blisters, HIC, SOHIC, distortion, crack-like flaws, creep, dent and gouges, laminations, wall thinning, cracking, embrittlement and mechanical damage
- Employ FFS procedures and level of assessment covering ASME FFS-1/API-579 procedure, API/ASME FFS levels of assessment, general FFS assessment procedure and failure prevention
- Review piping codes B31, boiler and pressure vessel code sections, storage tanks, other codes and standards, post-construction codes and design margin piping systems
- Discuss FFS of pipeline, piping, PV and tank
- Apply systematic assessment of existing equipment for brittle fracture
- Identify brittle fracture features, brittle fracture and material behavior, brittle fracture risk factors and safeguards against brittle fracture
- Measure toughness visually and discuss critical exposure temperature, applicability and limitations of the procedure and data requirements
- Carryout assessment techniques and acceptance criteria as well as remaining life assessment acceptability for continued service
- Assess general metal loss and recognize its applicability, limitations and inspection data/thickness measurements
- Apply UT measurements, check burst prevention and perform NDE data mapping and visual examination



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- Assess local thin area as well as apply thickness readings, stress analysis and piping assessment
- Employ proper assessment of pitting corrosion, laminations, weld misalignment, shell distortion, dents, gouges, crack-like flaws, creep and fire damage
- Carryout fitness for service assessment for a drilling platform structure and piping following fire damage
- Perform assessment of hydrogen blisters and hydrogen damage as well as fatigue and API 574 piping inspection
- Employ risk-based inspection, inspection planning and equipment screening

Exclusive Smart Training Kit - H-STK®



Participants of this course will receive the exclusive "Haward Smart Training Kit" (**H-STK**[®]). The **H-STK**[®] consists of a comprehensive set of technical content which includes **electronic version** of the course materials conveniently saved in a **Tablet PC**.

Who Should Attend

This course provides an overview of all significant aspects and considerations of fitness-for-service (FFS) of process plant equipment, pressure vessels, piping and storage facilities in accordance with API 579-1/ASME FFS-1 standard. Integrity assessment engineers, maintenance engineers, specialists, site inspection engineers, piping engineers, mechanical engineers, plant engineers, engineers and other technical staff will benefit from the practical approach of this course. The course will also be very useful to those who are responsible in maintaining the integrity of process plant equipment and piping.

Course Fee

US\$ 5,500 per Delegate + **VAT**. This rate includes H-STK[®] (Haward Smart Training Kit), buffet lunch, coffee/tea on arrival, morning & afternoon of each day.

Training Methodology

All our Courses are including **Hands-on Practical Sessions** using equipment, State-of-the-Art Simulators, Drawings, Case Studies, Videos and Exercises. The courses include the following training methodologies as a percentage of the total tuition hours:-

30% Lectures

- 20% Practical Workshops & Work Presentations
- 30% Hands-on Practical Exercises & Case Studies
- 20% Simulators (Hardware & Software) & Videos

In an unlikely event, the course instructor may modify the above training methodology before or during the course for technical reasons.



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Course Certificate(s)

(1) Internationally recognized Competency Certificates and Plastic Wallet Cards will be issued to participants who completed a minimum of 80% of the total tuition hours and successfully passed the exam at the end of the course. Certificates are valid for 5 years.

Recertification is FOC for a Lifetime.

Sample of Certificates

The following are samples of the certificates that will be awarded to course participants:-







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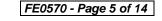




(2) Official Transcript of Records will be provided to the successful delegates with the equivalent number of ANSI/IACET accredited Continuing Education Units (CEUs) earned during the course.

H	Contin	uing Professional D	ogy Middle East evelopment (HTME-CPD) Script of Recoi	CI rds	
TOR IssuanceD HTME No. Participant Nam	8667-2014	4-9020-2559			
Program Ref.	Program	n Title	Program Date	No. of Contact Hours	CEU's
FE0570	API 579-1/ASME Service (FFS) of Proce Pressure Vessels, Facilities	ess Plant Equipment,	November 10-14, 2021	28	2.8
Total No. of CF	-I I's Famed as of TOR Is	ssuance Date			28
Total No. of CE	EU's Earned as of TOR Is	ssuance Date		TRUE COPY Jaryl Castillo Jaryl Castillo	2.8
Haward Technolo (IACET), 2201 Co with the ANSIIA Provider member Standard. Haward Technolo Education Units (IACET is an inter	gy has been approved as a operative Way. Suite 600, Herndon CET 1-2013 Standard which is ship status, Haward Technolog rgy's courses meet the profic CEUs) in accordance with the r	an Authorized Provider by n, VA 20171, USA. In obtain widely recognized to offer I essional certification and o ules & regulations of the In p programs according to stri	The International Association for Coo ng this approval, Haward Technology tandard of good practice internationally. AQCET CEUs for programs that qualify continuing education for Continuing etu-restor-based criteria and guideline	Juryl Castillo cademic Director	Training somplies thorized 1-2013 ntlinuing IACET).









Certificate Accreditations

Certificates are accredited by the following international accreditation organizations: -

The International Accreditors for Continuing Education and Training (IACET - USA)

Haward Technology is an Authorized Training Provider by the International Accreditors for Continuing Education and Training (IACET), 2201 Cooperative Way, Suite 600, Herndon, VA 20171, USA. In obtaining this authority, Haward Technology has demonstrated that it complies with the **ANSI/IACET 2018-1 Standard** which is widely recognized as the standard of good practice internationally. As a result of our Authorized Provider membership status, Haward Technology is authorized to offer IACET CEUs for its programs that qualify under the **ANSI/IACET 2018-1 Standard**.

Haward Technology's courses meet the professional certification and continuing education requirements for participants seeking **Continuing Education Units** (CEUs) in accordance with the rules & regulations of the International Accreditors for Continuing Education & Training (IACET). IACET is an international authority that evaluates programs according to strict, research-based criteria and guidelines. The CEU is an internationally accepted uniform unit of measurement in qualified courses of continuing education.

Haward Technology Middle East will award **3.0 CEUs** (Continuing Education Units) or **30 PDHs** (Professional Development Hours) for participants who completed the total tuition hours of this program. One CEU is equivalent to ten Professional Development Hours (PDHs) or ten contact hours of the participation in and completion of Haward Technology programs. A permanent record of a participant's involvement and awarding of CEU will be maintained by Haward Technology. Haward Technology will provide a copy of the participant's CEU and PDH Transcript of Records upon request.

• *** BAC

British Accreditation Council (BAC)

Haward Technology is accredited by the **British Accreditation Council** for **Independent Further and Higher Education** as an **International Centre**. BAC is the British accrediting body responsible for setting standards within independent further and higher education sector in the UK and overseas. As a BAC-accredited international centre, Haward Technology meets all of the international higher education criteria and standards set by BAC.

Accommodation

Accommodation is not included in the course fees. However, any accommodation required can be arranged at the time of booking.



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Course Instructor(s)

This course will be conducted by the following instructor(s). However, we have the right to change the course instructor(s) prior to the course date and inform participants accordingly:



Mr. Steve Magalios, CEng, PGDip (on-going), MSc, BSc, is a Senior Welding & Pipeline Engineer with almost 40 years of extensive Onshore/Offshore experience in the Oil & Gas, Construction, Refinery and Petrochemical industries. His expertise widely covers in the areas of Welding Technology, Welding & Fabrication, Welding Inspection, Pipeline Operation & Maintenance, Pipeline Design & Construction, Pipeline Repair Methods, Pipeline Engineering, Pipeline Integrity Management System (PIMS), Pipeline Pigging, Piping & Pipe Support Systems, Piping Systems & Process Equipment, Piping System Repair

& Maintenance, Piping Integrity Management, Computer Aided Design (CAD), Building & Road Design Skills, Civil Engineering Design, Structural Reliability Engineering, Road Construction & Maintenance, Concrete Structures & Building Rehabilitation, Reinforced Concrete Structures Protection, Geosynthetics & Ground Improvement Methods, Blueprint Reading & Interpretation, Blue Print Documentation, Mechanical Drawings, P&ID, Flow Diagram Symbols and Land Surveying & Property Evaluation. He is also wellversed in Lean & Sour Gas, Condensate, Compressors, Pumps, Flare Knockout Drum, Block Valve Stations, New Slug Catcher, Natural Gas Pipeline & Network, Scraper Traps, Burn Pits, Risk Assessment, HSE Plan & Procedures, Quality Plan & Procedures, Safety & Compliance Management, Permit-to-Work Issuer, ASME, API, ANSI, ASTM, BS, NACE, ARAMCO & KOC Standards, MS Office tools, AutoCAD, STAAD-PRO, GIS, ArcInfo, ArcView, Autodesk Map and various programming languages such as FORTRAN, BASIC and AUTOLISP. Currently, he is the Chartered Professional Surveyor Engineer & Urban-Regional Planner wherein he is deeply involved in providing exact data, measurements and determining properly boundaries. He is also responsible in preparing and maintaining sketches, maps, reports and legal description of surveys.

During his career, Mr. Magalios has gained his expertise and thorough practical experience through challenging positions such as a **Project Site Construction Manager**, **Construction Site Manager**, **Project Manager**, **Deputy PMS Manager**, **Head of the Public Project Inspection Field Team**, **Technical Consultant**, **Senior Consultant**, **Consultant/Lecturer**, **Construction Team Leader**, **Lead Pipeline Engineer**, **Project Construction Lead Supervising Engineer**, **Lead Site Engineer**, **Senior Site Engineer**, **Welding Engineer**, **Lead Engineer**, **Senior Site Engineer**, **R.O.W. Coordinator**, **Site Representative**, **Supervision Head** and **Contractor** for international Companies such as the Penspen International Limited, Eptista Servicios de Ingeneria S.I., J/V ILF Pantec TH. Papaioannou & Co. – Emenergy Engineering, J/V Karaylannis S.A. – Intracom Constructions S.A., Ergaz Ltd., Alkyonis 7, Palaeo Faliro, Piraeus, Elpet Valkaniki S.A., Asprofos S.A., J/V Depa S.A. just to name a few.

Mr. Magalios is a **Registered Chartered Engineer** and has **Master** and **Bachelor** degrees in **Surveying Engineering** from the **University of New Brunswick**, **Canada** and the **National Technical University of Athens**, **Greece**, respectively. Further, he is currently enrolled for **Post-graduate** in **Quality Assurance** from the **Hellenic Open University**, **Greece**. He has further obtained a Level 4B Certificates in Project Management from the National & Kapodistrian University of Athens, Greece and Environmental Auditing from the Environmental Auditors Registration Association (EARA). Moreover, he is a **Certified Instructor/Trainer**, a **Chartered Engineer** of Technical Chamber of Greece and has delivered numerous trainings, workshops, seminars, courses and conferences internationally.



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Course Program

The following program is planned for this course. However, the course instructor(s) may modify this program before or during the course for technical reasons with no prior notice to participants. Nevertheless, the course objectives will always be met:

<u>Day 1:</u>	Sunday, 28 th of July 2024
0730 – 0800	Registration & Coffee
0800 - 0815	Welcome & Introduction
0815 - 0830	PRE-TEST
	API 579-1 & ASME FFS-1 Standards API/ASME Standard API 579-1/ASME FFS-1 • ASME B31 Codes • ASME 331.3 Process Piping Code • Is fitness-for-service a code? • Standard • The
0830 – 0930	Inspection Drive Mechanisms • Why use a Fitness for Service Assessment? • Failure Conditions and Types of Flaws • Multidisciplinary Nature of FFS Assessment • Fitness-for-Service Assessment Procedure • Levels of Assessment • Evaluation Methodology • Typical Level 1 Limitations • Level 2 Assessment • Acceptance Criteria • Concept of Remaining Strength Factor (RSF) • Calculation of RSF for Corroded Cantilever Pipes with Increasing Corrosion Levels • Acceptance Criteria
0930 - 0945	Break
0945 – 1100	FFS & Degradation Mechanisms Benefits • Matching between Degradation Mechanisms and FFS Parts • Contents of ASME FFS-1/API 579 • ASME FFS-1/API 579 Contents • Brittle Fracture • General Metal Loss (GML) • Local Thin Area (LTA) • Pitting Corrosion • Blisters, HIC and SOHIC • Distortion • Crack-Like Flaws • Creep • Post-Fire • Dent and Gouges • Laminations • Annexes to ASME FFS-1 / API 579 • Plant Engineer Perspective • Wall Thinning • Cracking • Embrittlement • Mechanical Damage
1100 – 1200	FFS Procedures & Level of Assessment ASME FFS-1/API-579 Procedure • API/ASME FFS Levels of Assessment • General FFS Assessment Procedure • Conditions of Applicability • Design Margins for Each FFS Evaluation Level • Failure Prevention • Piping Codes B31 • Boiler & Pressure Vessel Code Sections • Storage Tanks • Other Codes and Standards • Post-Construction Codes • Design Margin Piping Systems • Case Study -1 • B31.3 Piping System • Parameters • Minimum Wall Thickness by Code (ASME B31.3) • Example • Next Three Steps • Design Margins in Piping Systems • Design Margin Pipelines • Design Margins Pressure Vessels (ASME B&PV)
1200 - 1215	Break
1215 – 1300	FFS of Pipeline, Piping, PV & Tank ASME B&PV Section II Part D • ASME II Part D • Case Study - 2: ASME VIII Div.1 • Minimum Wall Thickness by Code • Design Margins Tanks API 620-650 • Design Margins – Tanks • Case Study – 3 • Example • Weight Stress • Longitudinal Stress Equation • Weight Stress • Example: 10 in. NPS, sch.40 • Bending Stress Due to Sag • Review • The Inspector's Calc's • Exercises • Who is involved in Fitness-For-Service? • Objectives of FFS Assessment • Advantages of FFS Assessment • CSWIP Plant Inspection
	<i>Programme – Level 1, 2 and 3 • Resource Documents of FFS Standard</i>



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1300 - 1420	Assessment of Existing Equipment for Brittle Fracture Brittle Fracture • Level 1 Assessment – Applicability and Limitations • What is Brittle Fracture? • What is Brittle Failure • Identifying Brittle Fracture Features • Brittle Fracture and Material Behavior • Brittle Fracture Risk Factors • Safeguards Against Brittle Fracture • Repairs • Figure 3.1 Overall Brittle Assessment Procedure for Pressure Vessels and Piping (API RP 579) • Figure 3.2 Brittle Fracture Assessment for Storage Tanks (API 579) • Compare to Ductile Fracture • Characteristics of a Brittle Fracture • Toughness ASTM A 370 • Toughness of CS vs. SS • BCC Ferrite vs. FCC Austenite • C Content • Movement of Dislocations: Ductile • Carbon Atom Pins the Dislocation • Drop Weight Tear Test (DWTT) - ASTM E 436 (or API RP 5LR)
1420 - 1430	Recap Using this Course Overview, the Instructor(s) will Brief Participants about the Topics that were Discussed Today and Advise Them of the Topics to be Discussed Tomorrow
1430	Lunch & End of Day One

Day 2:	Monday, 29 th of July 2024
0730 - 0900	Assessment of Existing Equipment for Brittle Fracture (cont'd)Toughness Measured VisuallyCET - Critical Exposure TemperatureApplicability and Limitations of the ProcedureData RequirementsAssessment Techniques and Acceptance CriteriaRemaining Life AssessmentAcceptability for Continued ServiceToughness and HardnessRequirements for Low Temperature Toughness TestsCase Study 3-1Solution to Case Study 3-1 Assignment of Materials to Curves in Fig. 3.3Notes to Curves in Fig. 3.3Notes to Curves in Fig. 3.3Solution 3-1Solution to Case Study 3-1Material Groups TableASME B&PV Code, Section IXSolution to Case Study 3-2Case Study 3-3Case Study 3-4High-Pressure Purge VesselProcess Separator VesselPart 3 - Brittle Fracture AssessmentClass Quiz
0900 - 0915	Break
0915 – 1100	Assessment of General Metal Loss (GML)Two Failure Modes: Leak or Burst \bullet Part 4 General Metal Loss \bullet ASME -Three Levels for FFS \bullet Applicability and Limitations \bullet InspectionData/Thickness Measurements \bullet Point Thickness Readings Technique (API 579) \bullet Critical Thickness Profile (CTP)Technique \bullet Spacing of UT Point Readings \bullet Case Study - Storage Tank \bullet Tank Data \bullet ASTM A 283 C \bullet Shell ExternalCorrosion \bullet Shell Inspection \bullet Corrosion in the Tank Shell \bullet Meridional andCirc. Insp. Planes \bullet Inspection Grid \bullet Major Structural Discontinuity \bullet Thickness Measurements (in): 1" x 1" Grid \bullet Future Corrosion Allowance(FCA) \bullet Corrosion Rates: Rule of Thumb \bullet Applicability of GML Part 4 \bullet Conclusion \bullet Case Study – Pressure Vessel \bullet Case Study COV > 10%Vessel Data



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1100 - 1215	Assessment of General Metal Loss (GML) (cont'd)UT Measurements• UT Measurements at 1" Spacing• Check BurstPrevention• Assignment• NDE Data• Mapping• Screening• FFSReports• Caution: Discontinuities• Caution: Buckling• Level 3 Analysis•Assignment• Input Data• UT Readings are 2 in. Apart• Review• HeatExchanger Tube Bundle• HX Data• Inspection Planning• Risk-BasedInspection Sample• Inspection Sampling• Inspection Techniques• Visualexamination• When to plug• Replacement Practice• FFS Assessment•Review
1215 - 1230	Break
1215 - 1315	Assessment of Local Thin Area (LTA) Local Thin Areas (LTA's) • Starting Point ASME B31G • B31G Table • Folias' Formula • Three Assumptions • Case Study 1 • Case Study 2 – Evaluate Level 1 • Conclusions and Options • Supplemental Case Study: SS- Lined Tank • Level 3 - Section of Vacuum Tower
1315 - 1420	Assessment of Local Thin Area (LTA) (cont'd)Thickness ReadingsDescriptionStress-Strain Curve at 350° FStressAnalysis of Vacuum TowerAssignmentReview QuizAssessmentStress AnalysisLevel 1 Assessment
1420 - 1430	Recap Using this Course Overview, the Instructor(s) will Brief Participants about the Topics that were Discussed Today and Advise Them of the Topics to be Discussed Tomorrow
1430	Lunch & End of Day Two

Day 3:	Tuesday, 30 th of July 2024
0730 - 0900	Assessment of Pitting CorrosionAssessment of Pitting Corrosion • The 8 Standard Templates of Pitting Grades• Selection of Pitting Colonies • AP1579-1/ASME-FFS- 1 • Level 1Assessment • Determination of RSF using Pitting Grades Templates • Resultsof Level 1 Assessment • Case Study 1 • Question to be Resolved • Lowest PitDensity Chart • Highest Pit Density Chart • Interpolate for RSF •Conclusion • Level 2 Assessment • Determination of Pitting Couples •Results of Level 2 Assessment • Applicability of Level 2 • Level 3 Assessment(Nonlinear FEA) • FE Modelling for Pitted Pipe • Von-Mises StressDistributions from FEA • Distributions of Radial Deformation from FEA •Limit Pressures for Pitted Pipes by TES Method • Comparison between theResults Obtained using FEA and Part 6 of API-579/ASME-FFS-1 • Case Study2 • Input Parameters • Conclusions and Recommendations • Review
0900 - 0915	Break
0915 - 0945	Assessment of LaminationsCauses of LaminationsCase Study – Separator and Downstream ReactorLaminationGeneral ApproachDetection of LaminationsEquipment FailureAcoustic Emission (AE) TestingWhat is AcousticEmission (AE) Testing?Emission (AE) Testing
0945 - 1045	Assessment of Weld Misalignment & Shell DistortionDent• Weld Misalignment• Level I Assessment• ASME B31.3Fabrication Tolerance API 650 and 620• Level 2• Case Study 1•Assignment• Level 1 - B31.4 Oil Pipelines• Level 3 - FEA• Review



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	Assessment of Dents & Gouges
1045 1145	Definition of a Dent • Example of Dent • Pipeline Issue: Large PD/2t •
	Installation of Pipeline • Types of Dents • Kinked Dent • The Significance of
	Dents • ASME B31.8: Must Repair if • Dents on Weld Seams • Burst
	Strength of Dented Welds • Braga Noronha et. al. (Petrobras) • Measurements
1045 – 1145	0
	for a FFS Assessment • Fatigue Life of Dented Welds • Fatigue Check •
	Rebound Fatigue Test • Significance of Dents in Pipelines • Gouge • Gouge -
	Dent Combination • Recommendations for the Assessment of Dents •
	Assignment • Level 3 FEM
	Assessment of Crack-like Flaws
	Crack-Like: Incomplete Penetration • Fabrication Flaws • Crack-Like: Corrosion
	Cracking • Crack-Like: Fatigue Crack • Fatigue Crack • Fatigue Crack at
	Intersection • Fatigue Testing of Pipe Fittings • Crack-like Flaws • Cycles to
	Failure (Markl Tests) • Actual Failure vs. B31.3 Markl Limit SA • ASME
1145 – 1230	B&PV Design Fatigue Curves (CS in air) • API 579 Fatigue Curves • Running
1145 - 1250	Crack? • Introduction to Fracture Mechanics • Crack Opening Displacement
	(COD) • 1st Condition of Crack Stability • 2nd Condition of Crack Stability •
	Three Modes of Fracture • Stress Intensity – General Form • How to Obtain
	KIC (the stress intensity limit to start a crack in mode I)? • Three Assessment
	Levels • Complex Geometry • Crack from Expansion-Contraction • Liquid
	Penetrant Test (PT) of Crack • Case Study 9-1 • Corrosion Crack
1230 - 1245	Break
	Assessment of Crack-like Flaws (cont'd)
	Class Exercise 9-2 • Case Study 9-3 • Pipeline • Stress Ratio Lr • Stress
	Intensity K • Approximate Mode I Stress Intensity Factor at the Crack (KIC) •
	Lower Bound Ferritic Steels • Calculate Reference Temperature (Tref) • Figure
	3.4 (API RP 579, 2007) • Example: Stress Intensification Factor, Mode I (KIC) •
	Stress Intensity Ratio Kr • Failure Assessment Diagram (FAD) • How will the
1245 – 1400	Crack Size Progress? • Increment of Crack Growth for a Given Cycle (da/dN) •
1240 1400	da/dN , but ΔK is complex • Computational Fluid Dynamics (CFD) Simulation •
	Experimental Benchmark • Reactor Vessel Penetrations PWSCC • Control Rod
	Drive Mechanism (CRDM) Penetration • Stress Growth Velocity (da/dt) •
	Level 2 – Complete Analysis • Serious Complications for the Analysis • Leak-
	before-Break • Crack Stability Analysis • Level 3 - High Pressure Fitting • FFS
1400 - 1420	of Down-Comer Flaws Increasing Crack Depth (a) • Review Assessment of Creep
	What is Creep? • Creep Characteristics • The Three Creep Stages • Creep Machanism • Assessment of Creep Damage • Understanding the Effects of
	Mechanism • Assessment of Creep Damage • Understanding the Effects of
	Creep• Creep Strain at Constant Pressure • Creep Voids • Burst of
	Longitudinal Seam • Mohave Power Station, 1985:30 in. 600 psi @ 1000° F •
	Mohave Power Station, 1985 – Laughlin, Nevada • Δ Life vs. Δ Temperature •
	Temperature Profile is Critical • Remaining Life Assessment • Level 1 - Creep
	Assessment Procedure • Level 1 Assessment • Level 2 Assessment • Furnace
	Tube Example • Case Study 10-1 • Material • Measurement • Larson-Miller
	Parameter (LMP) • API 530 Larson-Miller Parameter (LMP) • Remaining Life
	Recap
1420 - 1430	Using this Course Overview, the Instructor(s) will Brief Participants about the
	Topics that were Discussed Today and Advise Them of the Topics to be Discussed
1400	
1430	Lunch & End of Day Three



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<u>Day 4:</u>	Wednesday, 31 st of July 2024
0730 - 0830	Assessment of Creep (cont'd)ReplicationWeld-O-Let Connections and Creep DamageCreep Failures• Comparison of Creep Stresses at 10,000 Hours for Various Special Alloys usedin High-Temperature ServiceWhat is Creep?Larson-Miller ParameterMPC Omega MethodModeling Creep BehaviorWhy Do Creep LifeAssessment?Inputs for Heater Tube AssessmentAPI 579-1 / ASME FFS-1 Creep Life AssessmentExample: Remaining Life ResultsWhy Do CreepTesting?Guidelines for Tube RemovalCoker HeatersCase Study:BackgroundCase Study: Omega vs. LMPOther Damage MechanismsCarburizationErosion• Challenges Predicting LifeReview QuizReview QuizComega
0830 – 0900	Assessment of Fire DamageFire DamageData RequirementsData Required for AssessmentDegradation Associated with HEZGeneral ApproachHeat ExposureHeat Exposure ZoneInspection TechniquesMeasurementsAssessmentTechniquesLevel I Assessment RepairsReplacementsCase StudyObservations from FireConclusionsActions
0900 - 0915	Break
0915 – 1000	Fitness for Service Assessment for a Drilling Platform Structure andPiping Following Fire DamageIntroduction • Fig.1. Consequences of Fire Damage • Fig.2. Identification ofthe 6 Heat Exposure Zones Level-1 Assessment • The Three Levels ofAssessment of Fire Damage • Specifications of Features of the 6 Fire Zones •Level-2 Assessment • Hardness Survey on Fire-Affected Piping • Results ofFFS Assessment • Pressure De-Rating of Heat Affected Piping • Outcomes ofFFS Assessment of Fire Damage
1000 - 1100	Assessment of Hydrogen Blisters & Hydrogen Damage Stress-Oriented Hydrogen Induced Cracking • Assessment of Blisters and Hydrogen Induced Cracking • Surface Bulging Due to Blisters • Detection, Characterization, and Sizing • Detection, Characterization, and Sizing of Blister Damage • Detection and Sizing of HIC Damage • Level I Acceptable if • Case Study 1 • Assignment Level 1 - Same Vessel • How to Prevent Hydrogen Blistering
1100 – 1200	Fatigue AssessmentFatigue Assessment•Level 1 Fatigue Assessment-Screening•Level 2Fatigue Assessment•Level 2 Fatigue Assessment Method C•Level 3Fatigue Assessment•Fatigue Assessment•Level 3
1200 - 1215	Break
1215 - 1420	API 574 Piping InspectionPiping Inspection Introduction• Basic Piping Inspection Program GoalsPressure Vessel Stress Areas• Basic Piping InspectionInspection for Corrosion
1420 - 1430	Recap Using this Course Overview, the Instructor(s) will Brief Participants about the Topics that were Discussed Today and Advise Them of the Topics to be Discussed Tomorrow
1430	Lunch & End of Day Four



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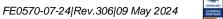




Day 5:	Thursday, 01 st of August 2024
0730 – 0815	API 574 Piping Inspection (cont'd)Selecting Corrosion Monitoring LocationsSystemBasic Piping InspectionPiping Injection Point ExamplePiping Injection Point Example 2
0815 – 0930	Risk-Based InspectionInspection PlanInspection TechniquesVisual ExaminationMagneticParticles Testing (MT)Yoke and Fluorescent MTMT: Advantages andLimitationsLiquid Penetrant Testing (PT)PT: Advantages andLimitations4. ReplicationRadiographic Testing (RT)RT: Advantagesand Limitations• RT Through Insulation• Digital Radiography•Ultrasonic Testing (UT)• Through-transmission Shear waves (angle beam)
0930 - 0945	Break
0945 – 1100	Risk-Based Inspection (cont'd)Classic Shear Wave Angle BeamPhased-ArrayLong Range Guided Wave(Ultrasound)Guided Wave TransducersCorroded Sphere Support LegsInspectionsResultsEddy Current Testing (EC)Eddy Current TestingPulsed Eddy CurrentMagnetic Flux LeakageInfrared ThermographyAcoustic Emission Testing (AE)AE: Advantages and LimitationsAEControlsLaser Mapping
1100 – 1200	Inspection PlanningWhat is RBI?Objectives of RBIRBI Benefits and LimitationsOutcomeof an RBI?International StandardsType of RBI AssessmentRBIPlanning Process OverviewData CollectionIdentification of DamageMechanismsProbability of FailureConsequence of FailureRiskAnalysisInspection PlanningMitigationReassessment and UpdatingRBI AssessmentsRBI SoftwaresRISKWISESystem OverviewRBIExample - Quantitative Assessment of a BoilerApplication SelectionCurrent TableItem ProposalItem PropertiesRisk FactorsRiskAnalysisLevel 1 AssessmentHomeUnit ProposalUnit AnalysisRBI ProcessRiskLikelihood x ConsequenceQualitative ApproachCUI LikelihoodRBI TeamLikelihood = Corrosion LoopsConsequence= Contents + Environment </td
1200 – 1215	Break
1215 – 1300	Equipment Screen Fluid Screen History Screen Scenarios Screen Actions Screen Mitigation Plan Likelihood = A (low) to E (high) Consequence = I (low) to IV (high) Risk-based Inspection Intervals Effective RBI Program Review
1300 - 1315	<i>Course Conclusion</i> <i>Using this Course Overview, the Instructor(s) will Brief Participants about the</i> <i>Course Topics that were Covered During the Course</i>
1315 - 1415	COMPETENCY EXAM
1415 - 1430	Presentation of Course Certificates
1430	Lunch & End of Course



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Simulator (Hands-on Practical Sessions)

Practical sessions will be organized during the course for delegates to practice the theory learnt. Delegates will be provided with an opportunity to carryout various exercises using the simulator "IntegriWISETM".



Course Coordinator

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